

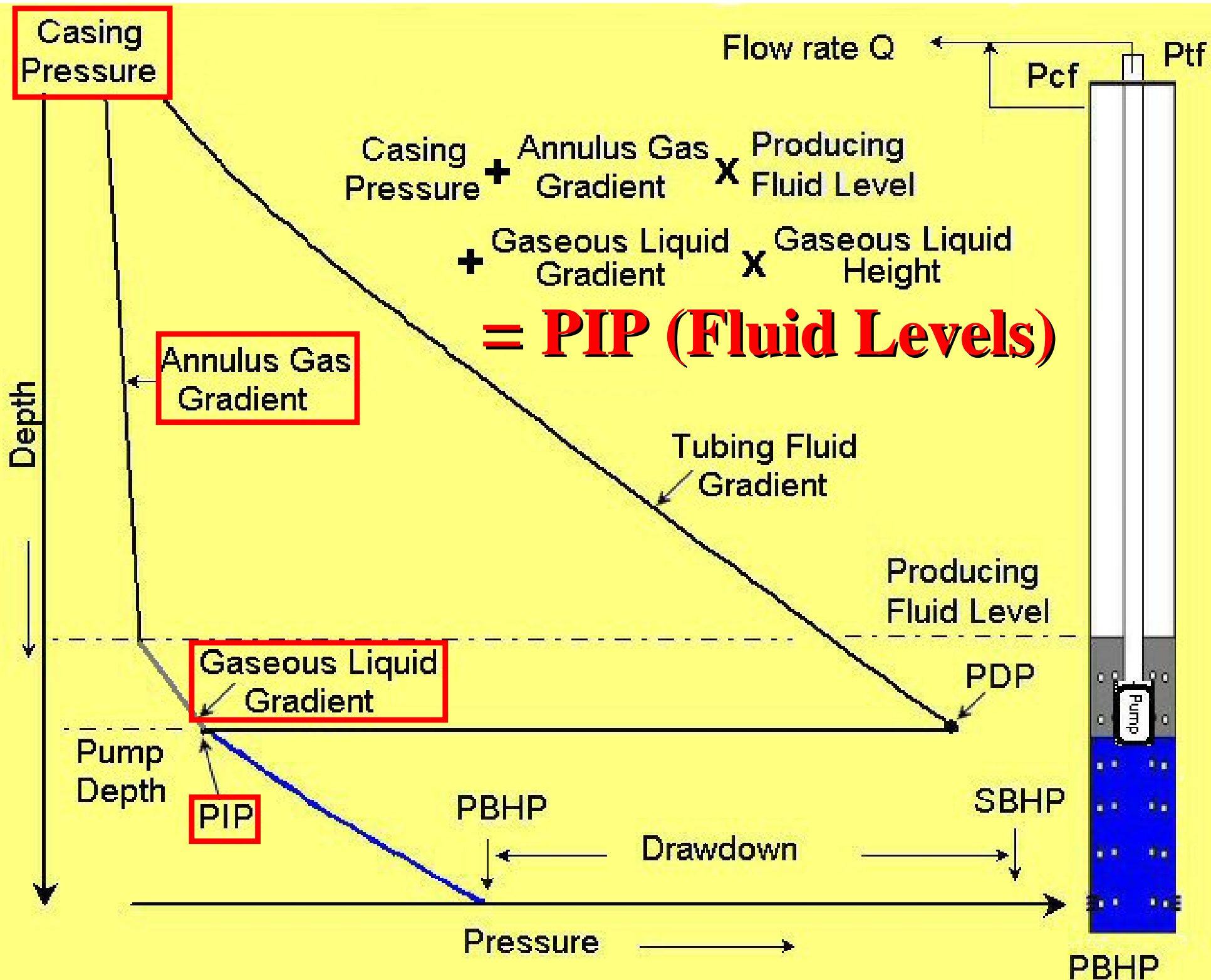
# **Dynamometer Analysis Advanced**

**Pump Intake Pressures from  
Dynamometer Pump Cards  
Valve Check Load Tests  
Fluid Levels Shots**

**(((ECHOMETER)))**

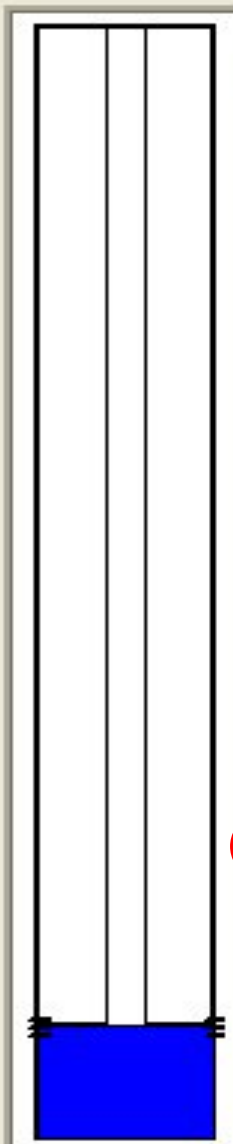
# Acoustic PIP Calculation

- ◆ Requires stabilized conditions
- ◆ Determination of Liquid Level Depth
  - Avg. Joint Length, Acoustic Velocity, SG Gas ....
- ◆ Measurement of casing pressure
- ◆ Tubing, Casing Size, & Pump Depth
- ◆ Oil, water and annular gas densities
- ◆ Measurement of casing pressure buildup rate (at Producing Conditions)



# Calculate Pump Intake Pressure from Fluid Level

Select Liquid Level	Depth Determination	Casing Pressure	<input checked="" type="checkbox"/> BHP	Collars
<b>Production</b>				
	Current	Potential		
Oil	18	18.2	BBL/D	
Water	38	38.4	BBL/D	
Gas	1.5	1.5	Mscf/D	
IPR Method: <input type="text" value="Vogel"/>				
PBHP/SBHP: <input type="text" value="0.05"/>				
Producing Efficiency: <input type="text" value="98.9"/> %				
<b>Fluid Densities</b>				
Oil	<input type="text" value="35"/>	deg.API		
Water	<input type="text" value="1.1"/>	Sp.Gr.H2O		
Gas Gravity	<input type="text" value="1.08"/>	Air = 1		
Acoustic Velocity: <input type="text" value="872.02"/> ft/s				
Casing Pressure: <input type="text" value="35.2"/> psi (g)				
Casing Pressure Buildup: <input type="text" value="0.3"/> psi				
: <input type="text" value="2.00"/> min				
Gas/Liquid Interface Pres.: <input type="text" value="42.1"/> psi (g)				
Liquid Level MD: <input type="text" value="3405.67"/> ft				
Formation Depth MD: <input type="text" value="3425.00"/> ft				
Well State: <input type="text" value="Producing"/>				
Annular Gas Flow: <input type="text" value="4"/> Mscf/D				
% Liquid: <input type="text" value="83"/>				
<b>Liquid Below Pump</b>				
Oil	<input type="text" value="0"/>	%		
Water	<input type="text" value="100"/>	%		
% Liquid Below Pump: <input type="text" value="100"/> %				
<input type="button" value="Liquid Below Pump..."/>				
Pump Intake Pressure: <input type="text" value="45.5"/> psi (g)				
PBHP: <input type="text" value="49.3"/> psi (g)				
Reservoir Pressure (SBHP): <input type="text" value="1340.3"/> psi (g)				
Pump Intake Depth (MD): <input type="text" value="3417.00"/> ft				
Total Gaseous Liquid Column HT (TVD): <input type="text" value="11"/> ft				
Equivalent Gas Free Liquid HT (TVD): <input type="text" value="9"/> ft				
Comment: <input type="text" value="Pumped off"/>				



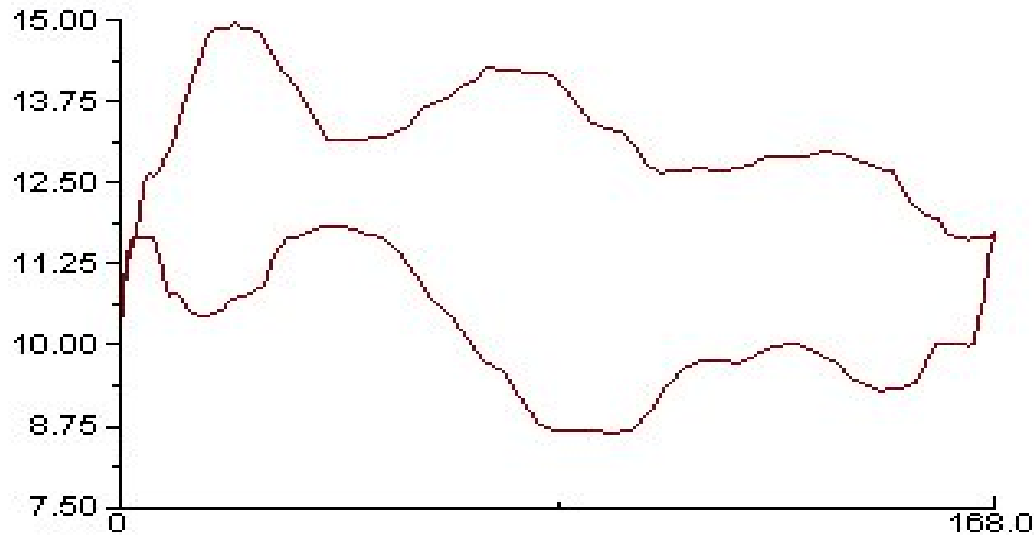
$$\text{PIP} = \text{Casing Pressure} + \text{Gas Gradient} * \text{Liquid Level} + \text{Gaseous (Gradient*Height)}$$

# **Dynamometer PIP Calculation**

- ◆ **Requires stabilized conditions**
- ◆ **Determination of Fluid Load**
  - » **Pump Card or (TV Load – SV Load)**
- ◆ **Measurement of tubing pressure**
- ◆ **Pump Diameter, Rod String & Pump Depth**
- ◆ **Oil, water and gas densities**
- ◆ **Oil, water, and gas Production Rate**
- ◆ **Damping Coefficients**

# Fluid Load, Fo, Has Two Reference Lines

Load (K-Lbs) vs Polished Rod Pos. (in)



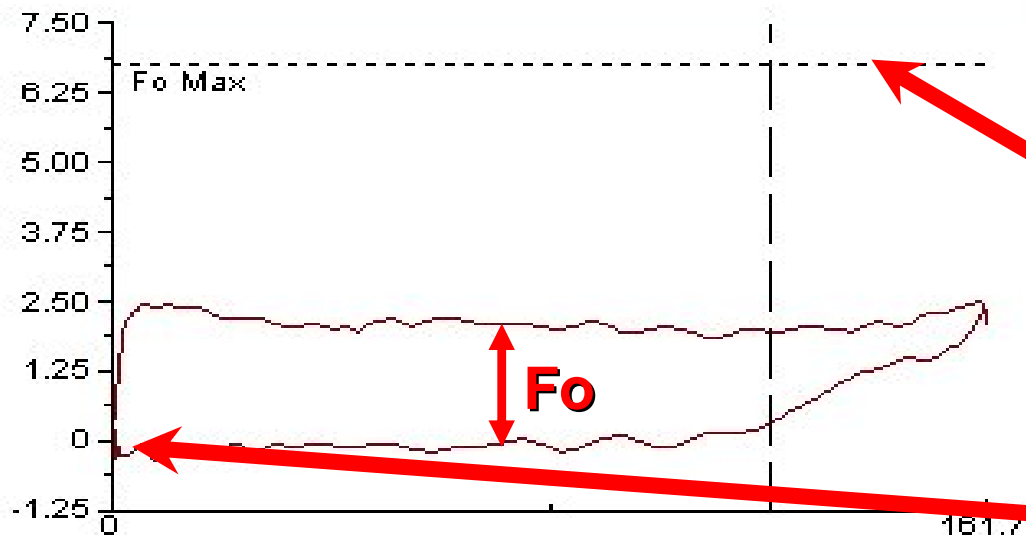
**Fo - Fluid Load is the load that the Pump applies to the rod string.**

$$F_o = F_{oUp} - F_{oDn}$$

Upstroke:  $F_{oUp} = (P_{dis} - P_{intk}) * A_p$

Downstroke:  $F_{oDn} = 0$

Load (K-Lbs) vs Plunger Pos. (in)

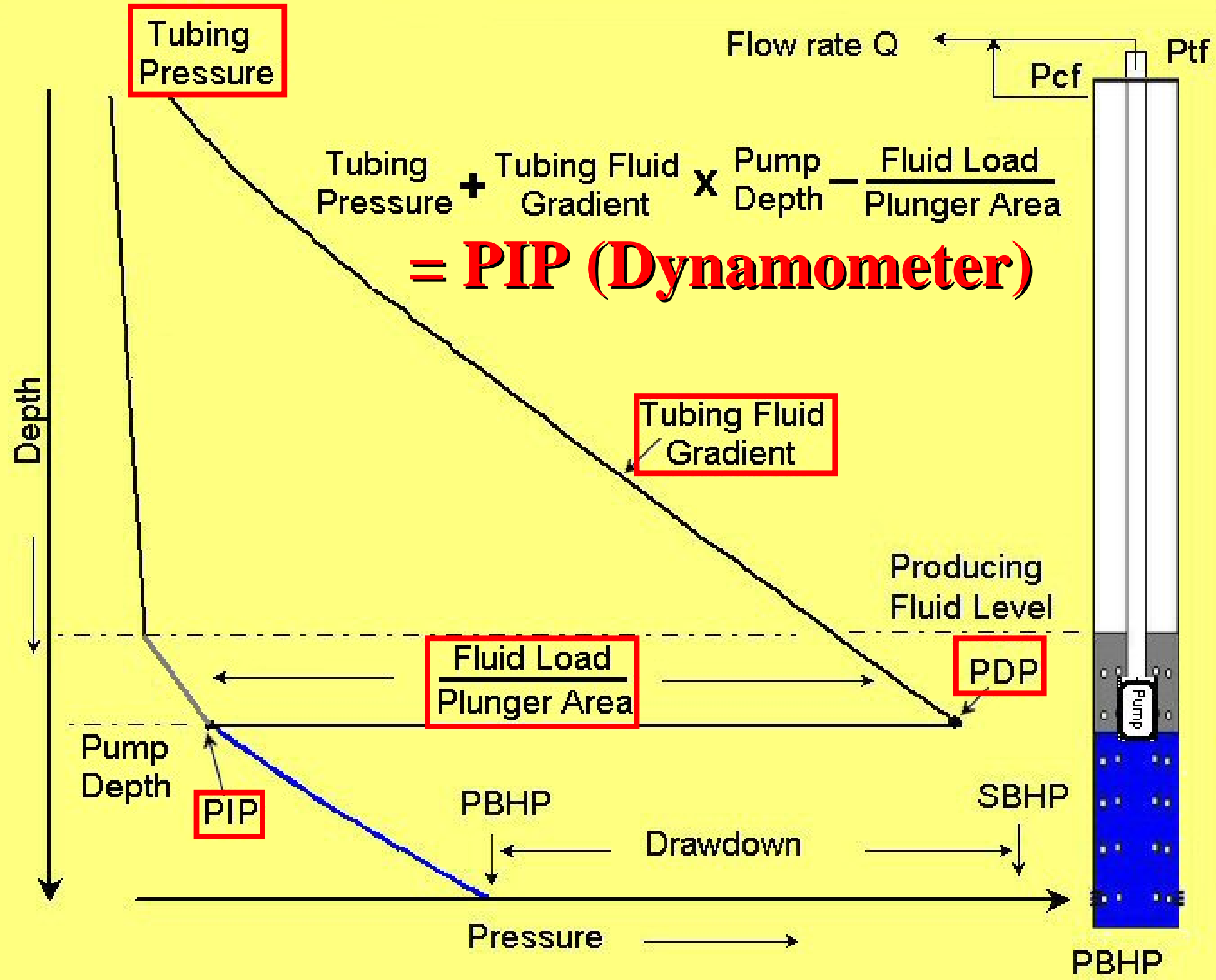


**Two reference lines**

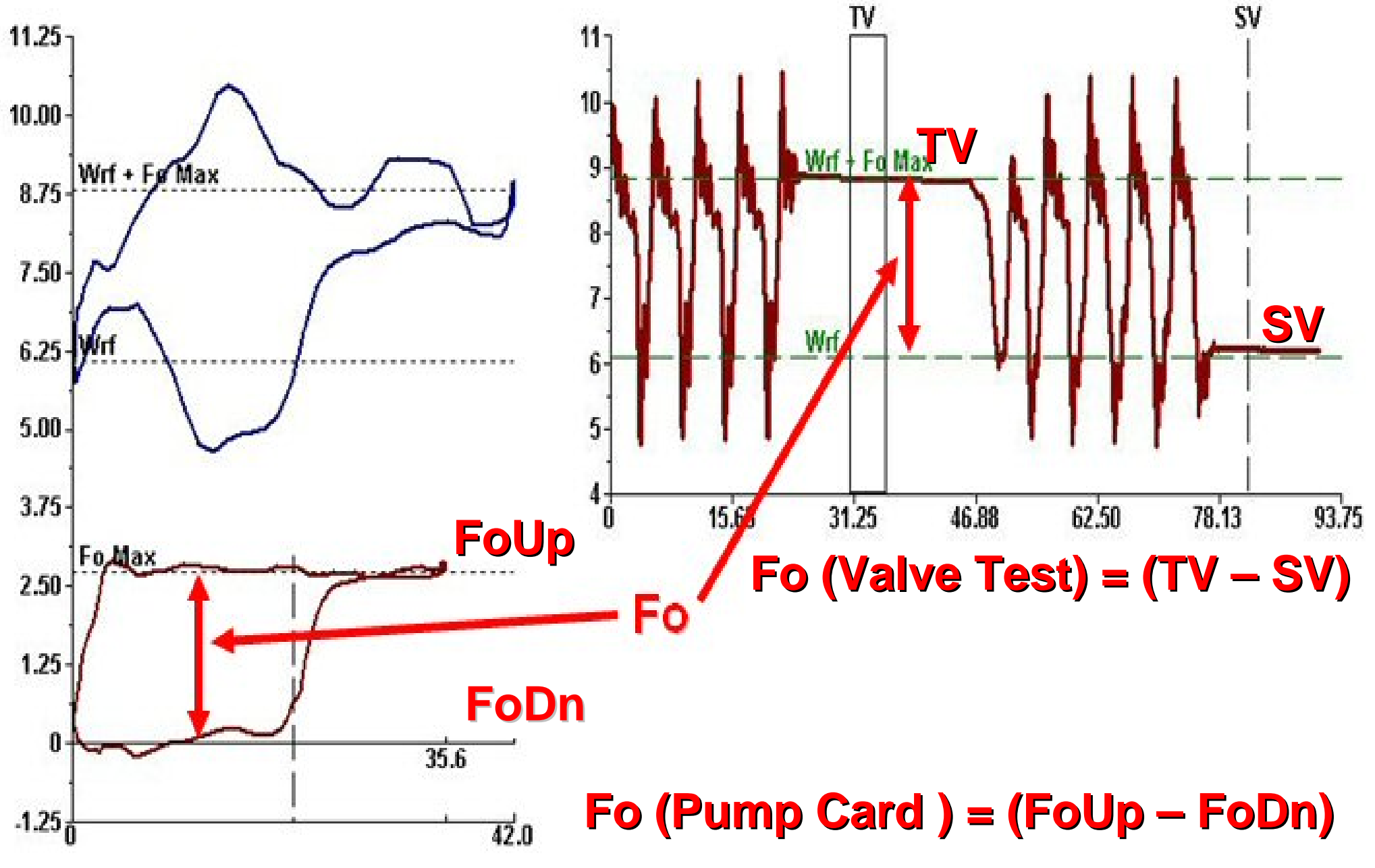
**1. FoMax = Pdis \* Ap**

FoMax is the maximum load that the pump would apply to the rod string assuming pump intake pressure is zero. The well provides no help in lifting the fluid to the surface.

**2. Zero Load Line**



# Calculate Pump Intake Pressure from Fluid Load



$PIP = \text{Tubing Pressure} + \text{Tubing Gradient} * \text{Pump Depth (TVD)} - Fo / \text{Plunger Area}$



# Calculate PIP using Fo from Pump Card

TWM - Examples : FluidPoundUnAnchoredTubing <Surface Card> acq-[04/20/96 01:49:00] Fluid Pound

File Mode Option Tools Help

Acquire Mode  
 Recall Mode

**F2** Data Files  
**F3** Select Test (P/C, DYN, ACU)  
**F4** Analyze

Raw Data | Errors/Warnings | Overlay |  Dyna Cards

Load(K-Lbs) vs Position (in)

Kr & Kt  lb/in    Kt  lb/in    Dyna Card Options...

Torque | Rod Loading | Analysis Plot

HLT024    PPRL     PPUMPL   
 MPRL     MPUMPL

Calculated Fluid Load Max  lb  
 Polished Rod Power  HP  
 Polished Rod / Motor Eff.  %  
 Strokes Per Minute

Pump Card HP  HP  
 Pump / Motor Eff.  %  
 Pump Displacement  BBL/D  
**Pump Intake Pressure...**  psi (g)

Damp Up   
 Damp Down     << Reset

Tubing Head Pressure  psi (g)

Effective Plunger Stroke  
         %     in   

Stroke     ?    < Pg Up    Pg Dwn >

# Calculate PIP using Fo from Pump Card

**Worksheet to Calculate Pump Intake Pressure using Fluid Load from Pump Card**

**Up Stroke Pump Load Options**

- Average of Up Stroke Loads
- Maximum Up Stroke Load ( adj. by Unaccounted Friction )
- Load at Pump Fillage Line
- User Input

Up    Down   

Fo Up  lb

**Calculations For Fo ( Fluid Load Plunger )**

Fo Calculated From PIP of Fluid Level Analysis  lb  
Fo = Plunger Area \* [ Tbg Pres. - PIP + Pump Depth \* Fluid Gradient ]

Fo Calculated from Valve Check Analysis  lb  
Fo = (TV-SV)

**Down Stroke Pump Load Options**

- Zero Load Line
- Minimum Down Stroke Load ( adj. by Unaccounted Friction )
- Average of Down Stroke Loads
- User Input

Up    Down   

Fo Down  lb

Unaccounted Friction  lb

Fo = FoUp - FoDown

Fluid Load (Fo)  lb

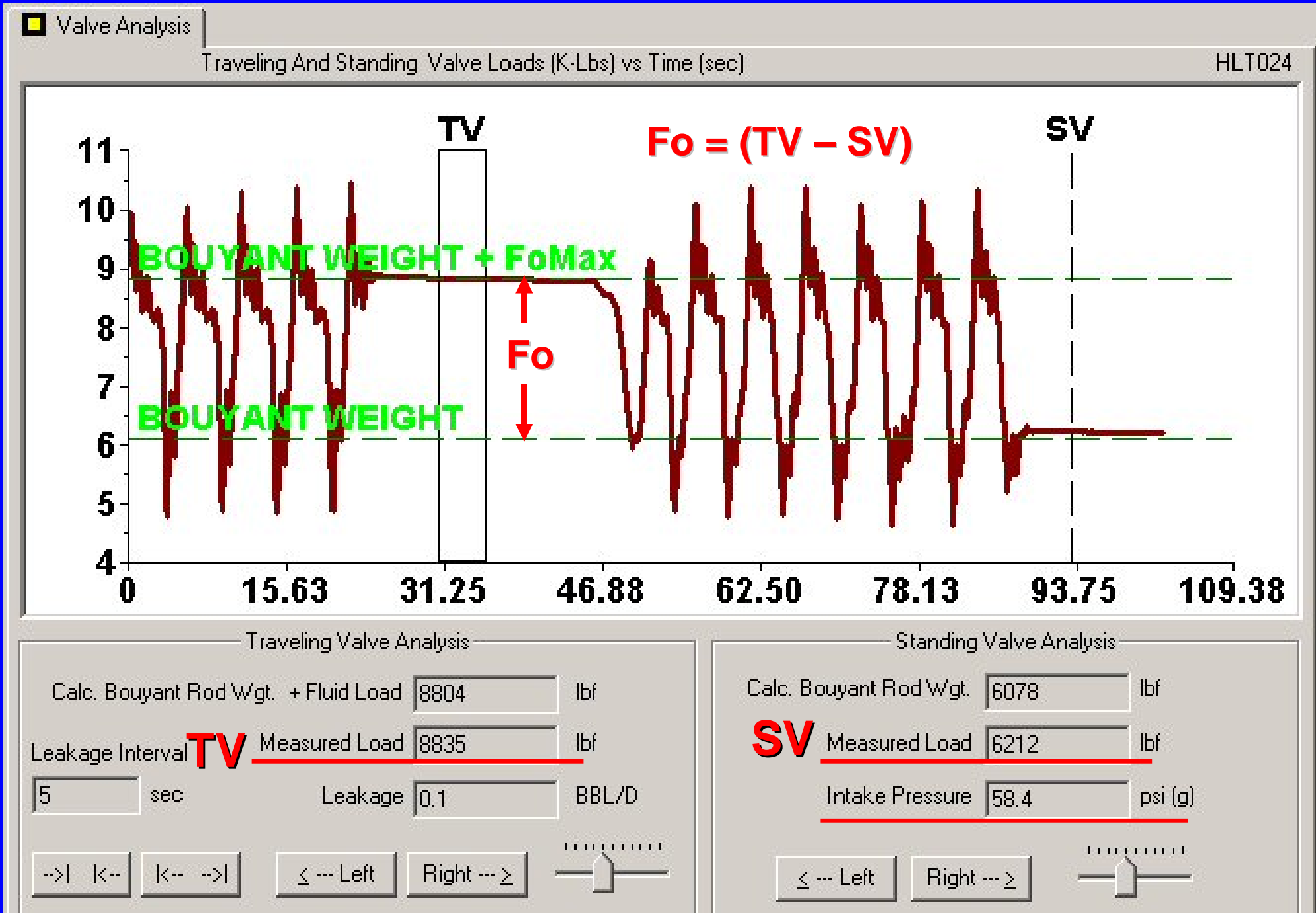
PIP = Tubing Pressure + Pump Depth(TVD) \* Fluid Gradient - Fo / Plunger Area

Pump Intake Pressure  psi

Include Worksheet In Reports

OK    Cancel

# Calculate PIP using Fo from Valve Test



# Well Data

## PIP Examples

- 1) Pump Cards
  - Valve Checks
  - Fluid Levels
  
- 2) Load Measured
  - a) Horseshoe
  - b) PRT
  - c) Modified Leutert
  
- 3) 16 selected from 38 possible files

#	Example Dataset Well Name	A	D	V
1	Anchored but NOT Set	1	L 1	✓
2	Anchored With Rod Stretch	✓	HT 47	✓
3	Asphaltenes in Pump	✓	L 2	✓
4	average_well	✓	PRT 1	✓
5	Bad Tail Bearing	✓	L 2 2	✓
6	Deep_well	✓	PRT 1	✓
7	FluidPoundUnAnchoredTubing	✓	L 2 1	✓
8	Flumping	✓	✓	
9	Gas Interference	✓	L 1	✓
10	GearboxBalance	✓	HT 1	✓
11	Gunk in Pump	✓	✓	
12	Leak Hole In Pump Barrel	✓	HT 1	✓
13	Leak Standing Valve	✓	PRT 1	✓
14	Leak Tubing Hole	✓	✓	✓
15	Leak TV Unanchored		✓	✓
16	Need Gas Separator	✓	HT 1	✓
17	PFL_Anomaly	✓	✓	
18	PFL_DHM_CasingWtChange	✓	HT 1	✓
19	PFL_DHM_CoalBedPerfs	✓	✓	
20	PFL_Gaseous_noisy	✓		
21	PFL_Gas lift	✓		
22	PFL_High	✓		
23	PFL_High_liquid_low_gas	✓		
24	PFL_Imp_Exp	✓		
25	PFL_Liner	✓	✓	
26	PFL_Lot of Gas2	✓	✓	
27	PFL_SBHP	✓		
28	PFL_Tubing_anchor	✓		
29	RodPart_5365		✓	
30	RodPart_NoPlunger		✓	✓
31	Tagging Down Hard	✓	PRT 1 26	✓
32	Tagging Fiberglass Rods on Downstroke	✓	HT 2 1	✓
33	Tagging Unanchored	✓	L 1	✓
34	Trash Sticks SV Open	✓	PRT 1 17	✓
35	Trash Sticks TV Open	✓	HT 1 12	✓
36	TV Action Erratic	✓	L 1	✓
37	Unaccounted Wellbore Friction	✓	HT 1	✓
38	V11	✓	HT 3 1	✓

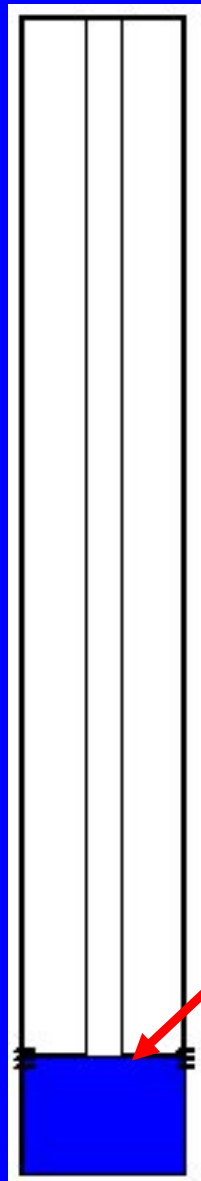
# Pump Intake Pressure from 16 Wells

- 1) Average Error (PIP – Avg) = 436.4 Psig
- 2) (Meas – Avg) / Avg = 7.7% – 123.4% Avg 64%
- 3) Pump Cards (3) Fluid Levels (5) Valve Check (8)

#	Example Dataset Well Name	DYNO Data	Pump Intake Pressure Psig			Average Psig	Error % (Meas - Avg)/Avg			Abs Max Error %	Abs Max Error Psig
			D	A	D		V	A	D		
38	V11	HT 3 1	62	66.2	42.7	57.0	8.8	16.2	-25.0	25.0	14.3
7	FluidPoundUnAnchoredTubing	L 2 1	45.4	109.9	58.4	71.2	-36.3	54.3	-18.0	54.3	38.7
9	Gas Interference	L 1	722.3	734.6	647.1	701.3	3.0	4.7	-7.7	7.7	54.2
33	Tagging Unanchored	L 1	62.9	53.6	187	101.2	-37.8	-47.0	84.8	84.8	85.8
16	Need Gas Separator	HT 1	228.4	117.3	271.9	205.9	10.9	-43.0	32.1	43.0	88.6
18	PFL_DHM_CasingWtChange	HT 1	286.5	386.3	550.4	407.7	-29.7	-5.3	35.0	35.0	142.7
32	Tagging Fiberglass Rods on Downstroke	HT 2 1	338.6	58.1	58.1	151.6	123.4	-61.7	-61.7	123.4	187.0
1	Anchored but NOT Set	L 1	400.3	65.3	165.3	210.3	90.3	-68.9	-21.4	90.3	190.0
5	Bad Tail Bearing	L 2 1	568.4	955	731.9	751.8	-24.4	27.0	-2.6	27.0	203.2
37	Unaccounted Wellbore Friction	HT 1	340.5	329.8	18	229.4	48.4	43.7	-92.2	92.2	211.4
2	Anchored With Rod Stretch	HT 47	176	118.3	542.7	279.0	-36.9	-57.6	94.5	94.5	263.7
10	GearboxBalance	HT 1	827.3	810.2	1649.4	1095.6	-24.5	-26.1	50.5	50.5	553.8
35	Trash Sticks TV Open	HT 1 12	305.1	364.7	1228	632.6	-51.8	-42.3	94.1	94.1	595.4
3	Asphaltenes in Pump	L 2	527	1545	1523	1198.3	-56.0	28.9	27.1	56.0	671.3
36	TV Action Erratic	L 1	622.7	2318.3	2303	1748.0	-64.4	32.6	31.8	64.4	1125.3
12	Leak Hole In Pump Barrel	HT 1	405.1	3989.8	4492.1	2962.3	-86.3	34.7	51.6	86.3	2557.2
			<u>5</u>	<u>3</u>	<u>8</u>				Average =	64.3	436.4
									Maximum =	123.4	2557.2
									Minimum =	7.7	14.3



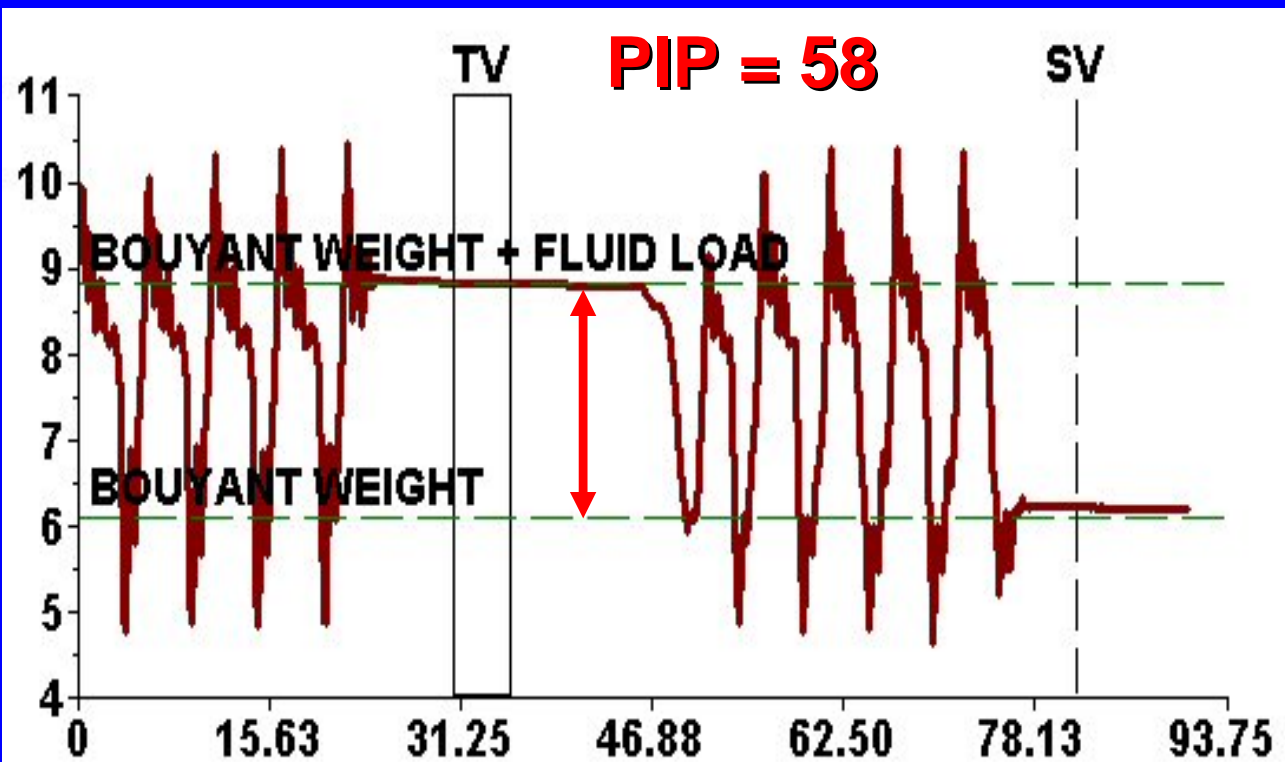
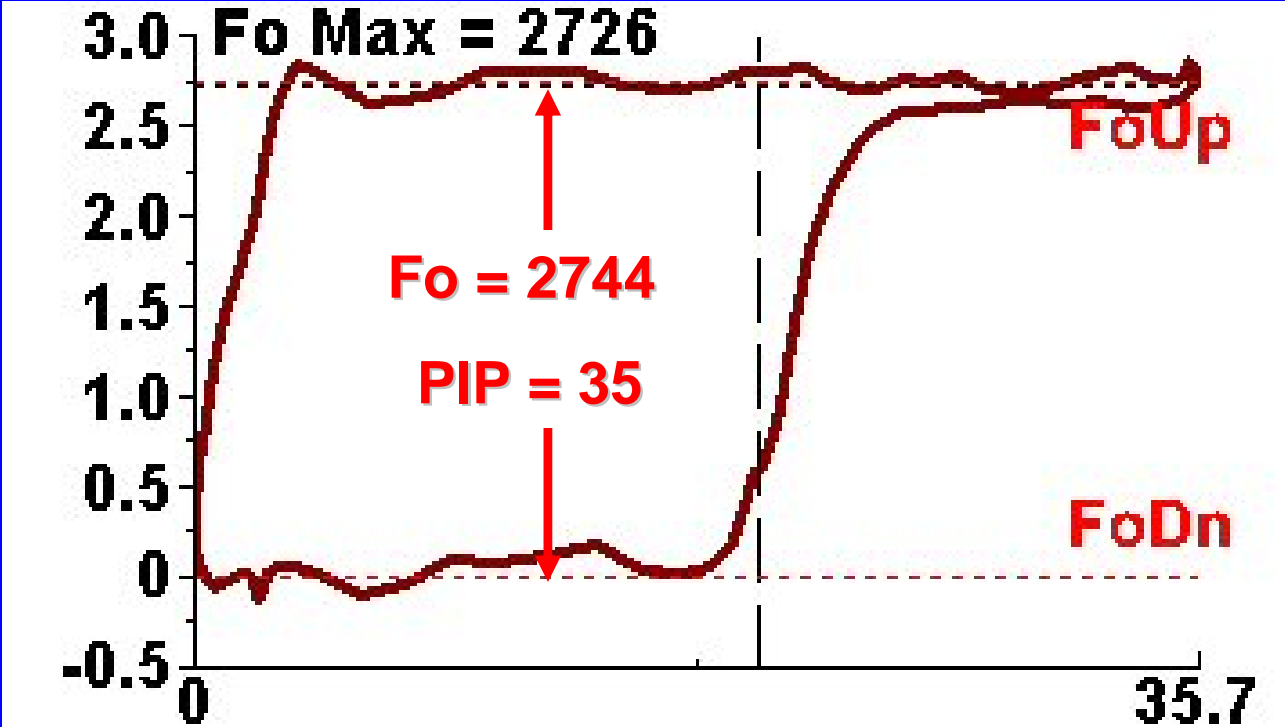
# 7 – Fluid Pound Unanchored Tbg



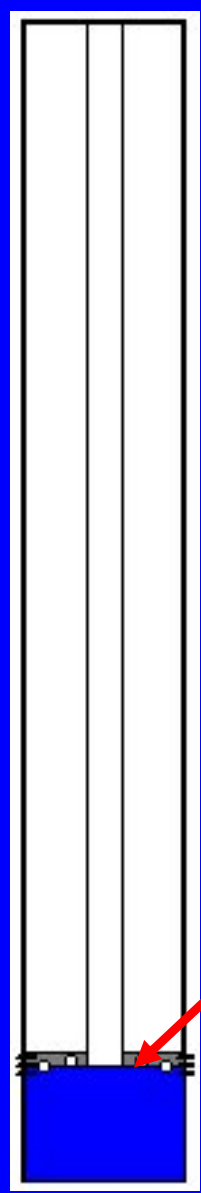
**1.5" = 1.78 in<sup>2</sup>**

**Fo(fl) = 2620**  
**Fo(pc) = 2744**  
**Fo(vc) = 2623**

**PIP = 45**



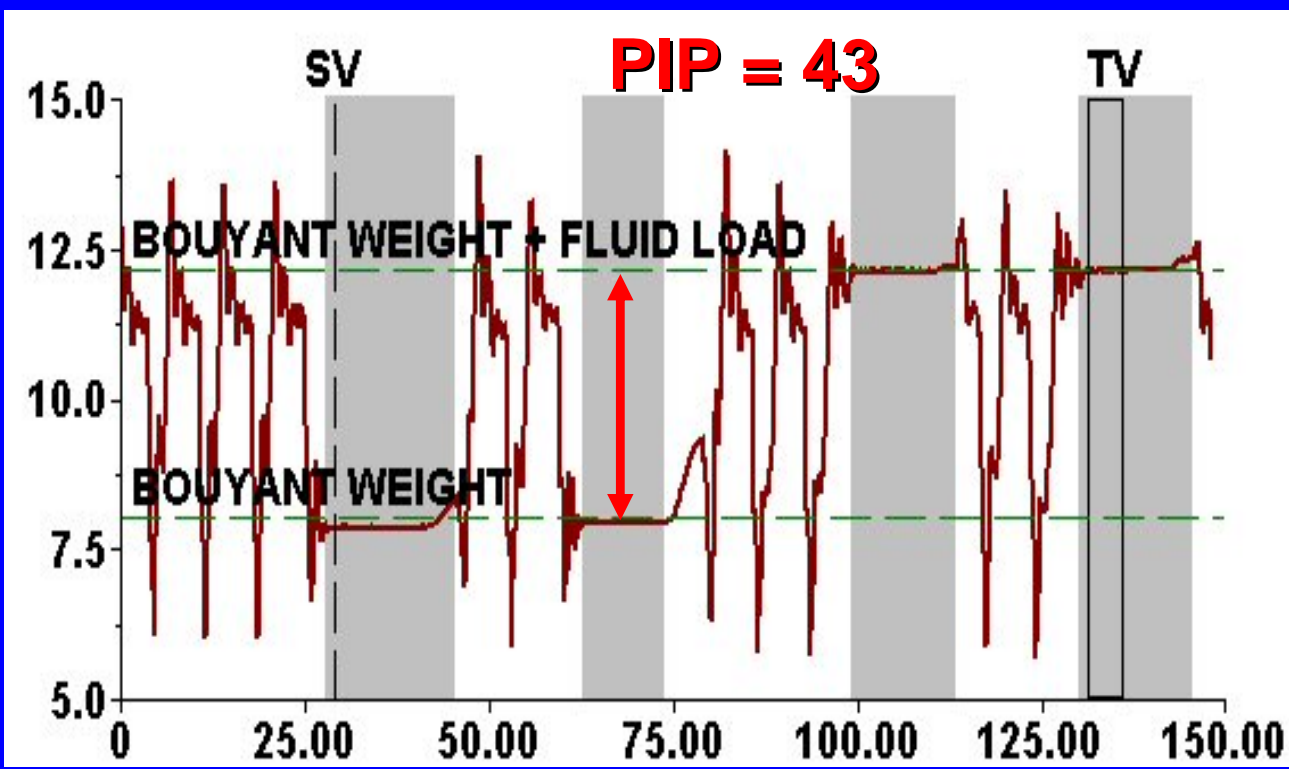
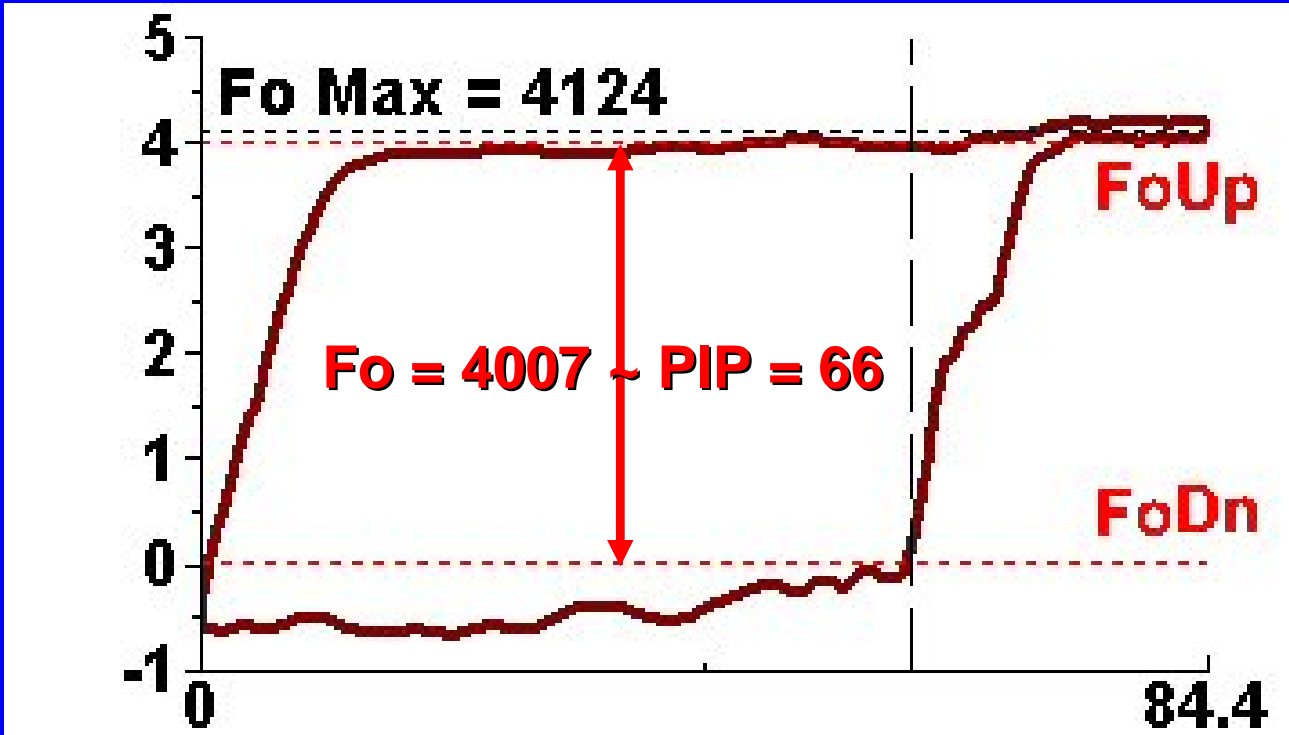
# 38 – V11 Normal Pumped Off Well



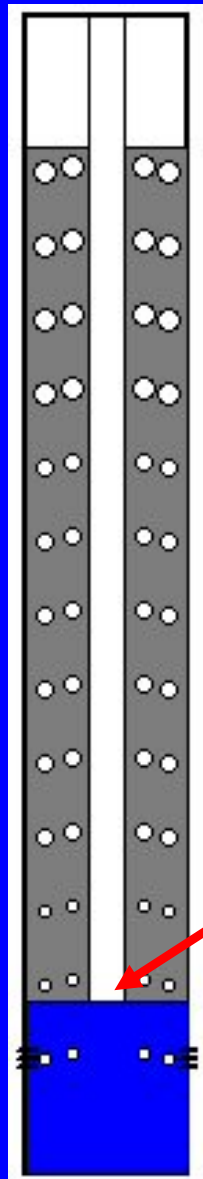
**1.5" = 1.78 in<sup>2</sup>**

**Fo(fl) = 3977**  
**Fo(pc) = 4007**  
**Fo(vc) = 4278**

**PIP = 62**



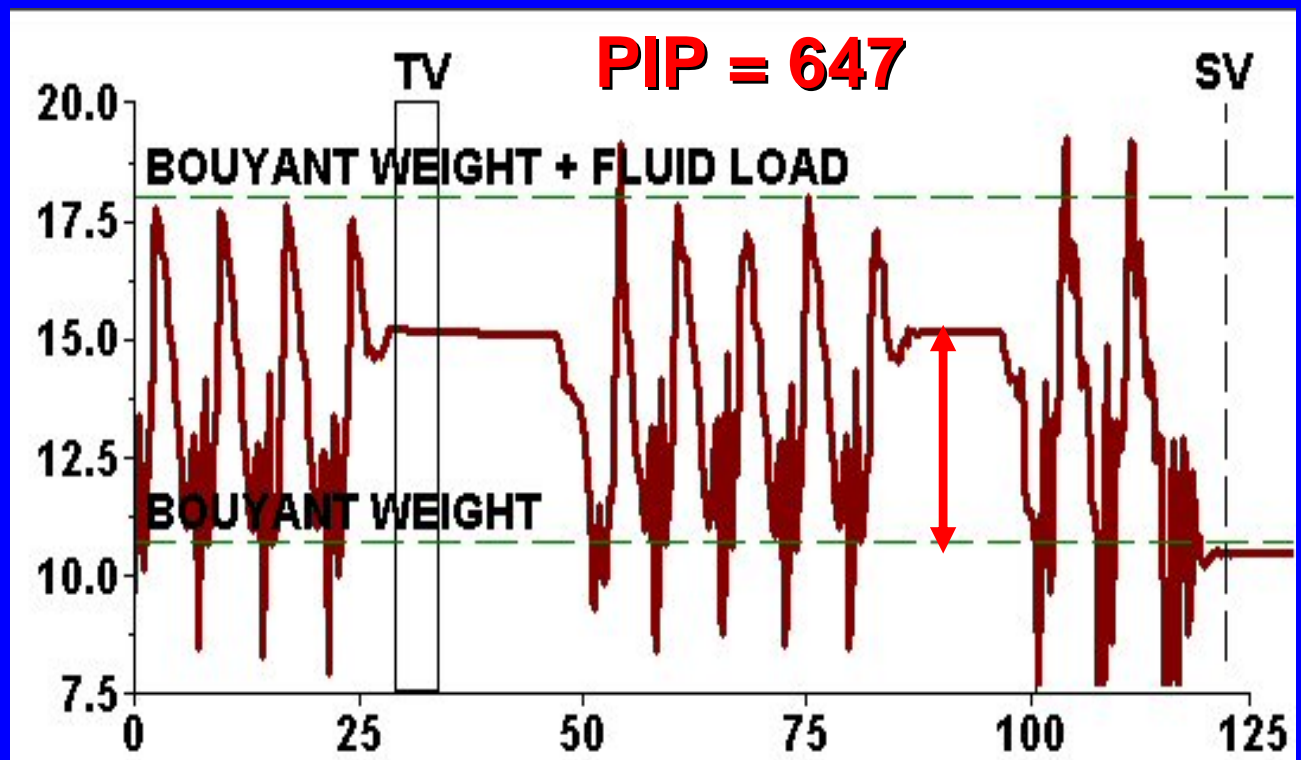
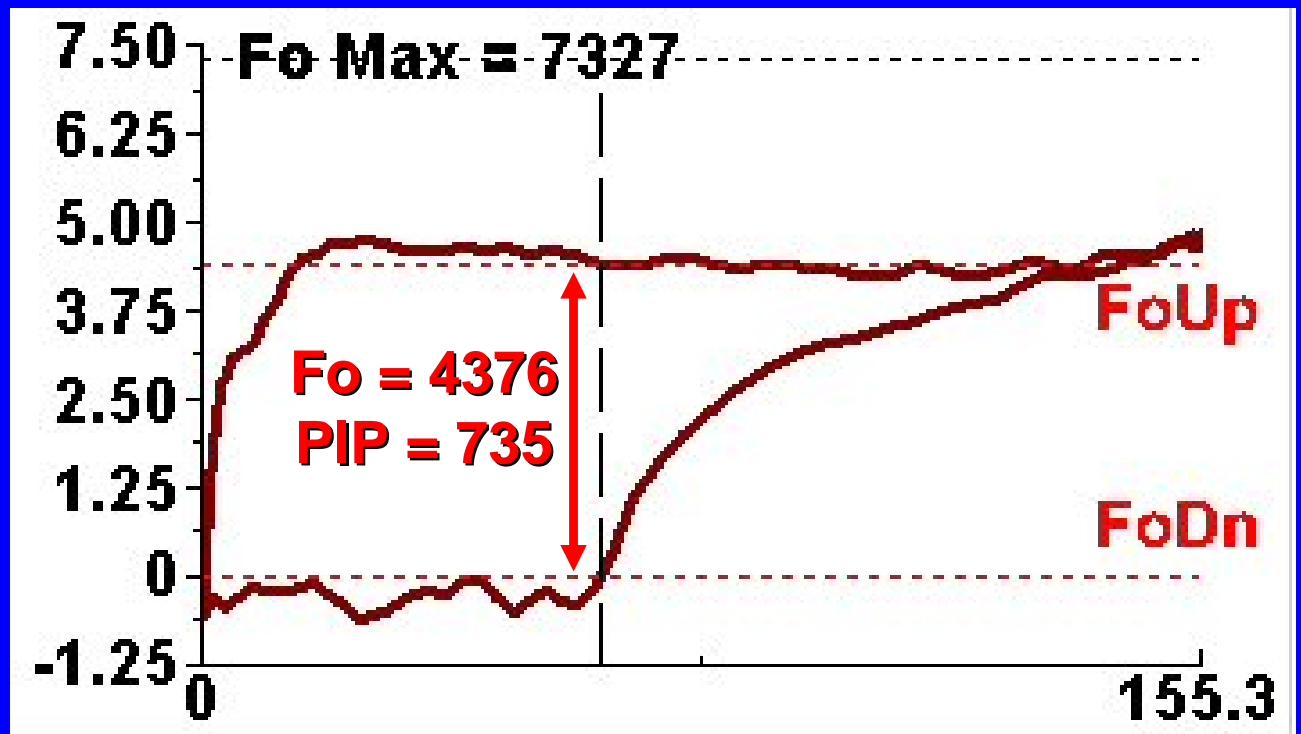
# 9 – Gas Interference



$2.25'' = 3.98 \text{ in}^2$

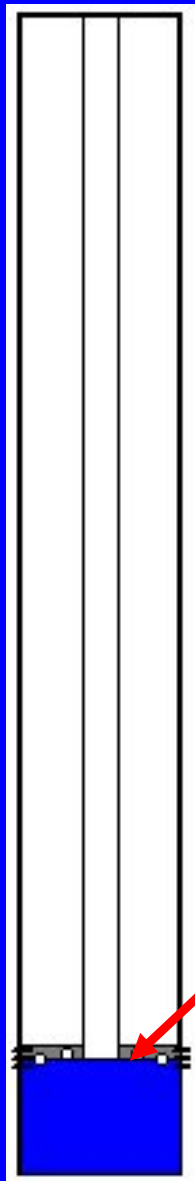
$Fo(fl) = 4399$   
 $Fo(pc) = 4376$   
 $Fo(vc) = 5045$

$PIP = 722$





# 35 – Trash Sticks TV Open



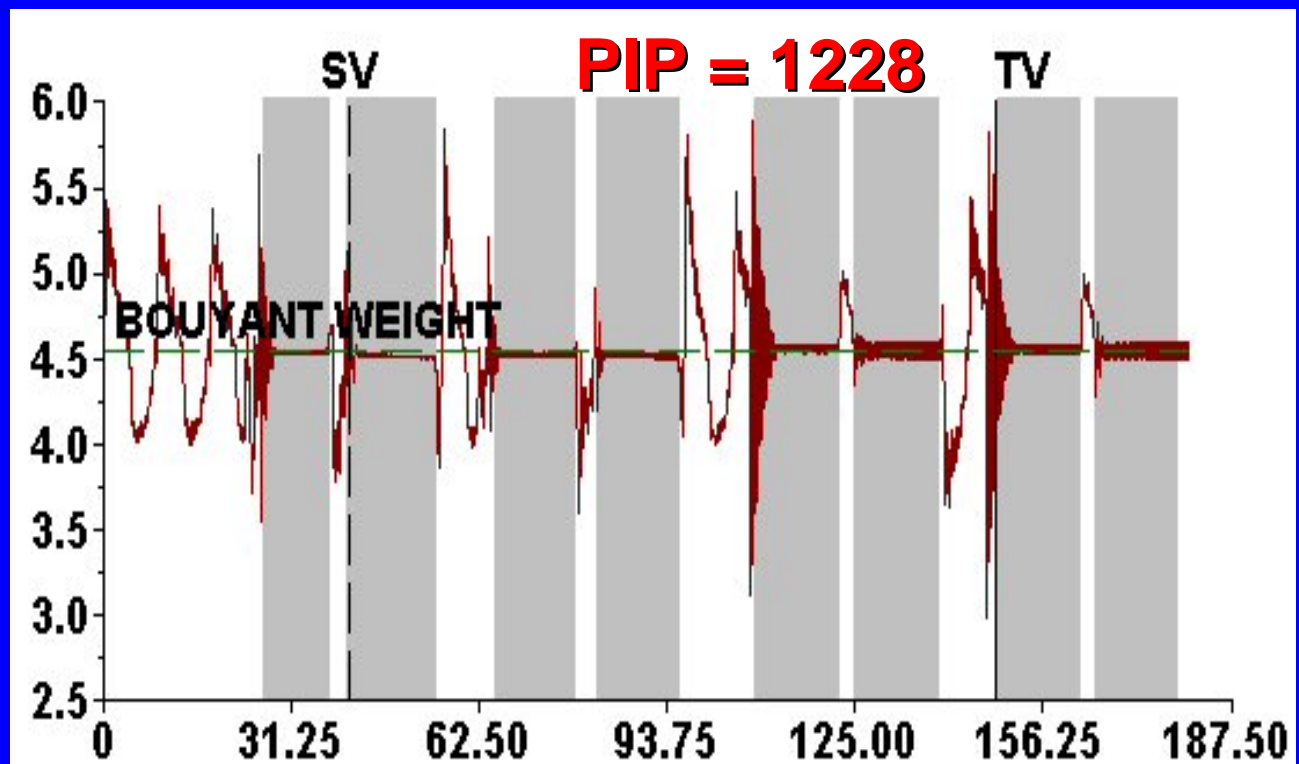
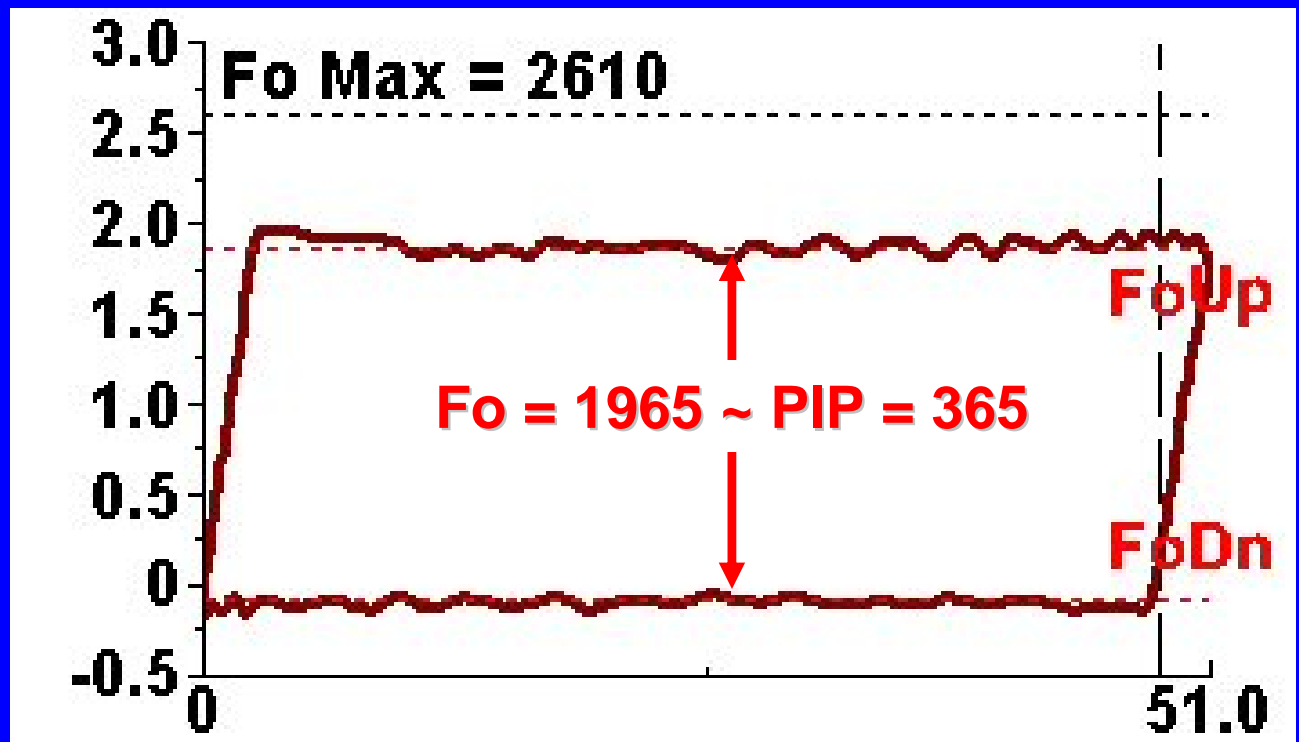
$1.5'' = 1.78 \text{ in}^2$

$Fo(fl) = 1962$

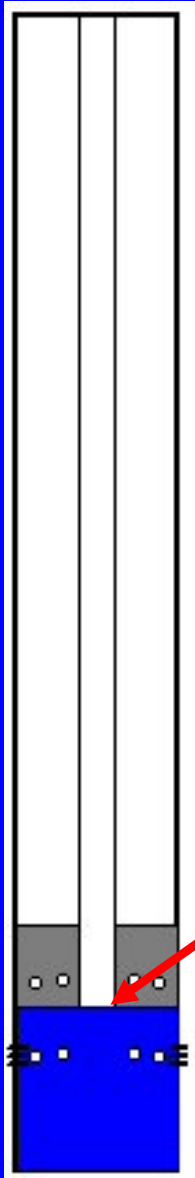
$Fo(pc) = 1965$

$Fo(vc) = 449$

$PIP = 352$

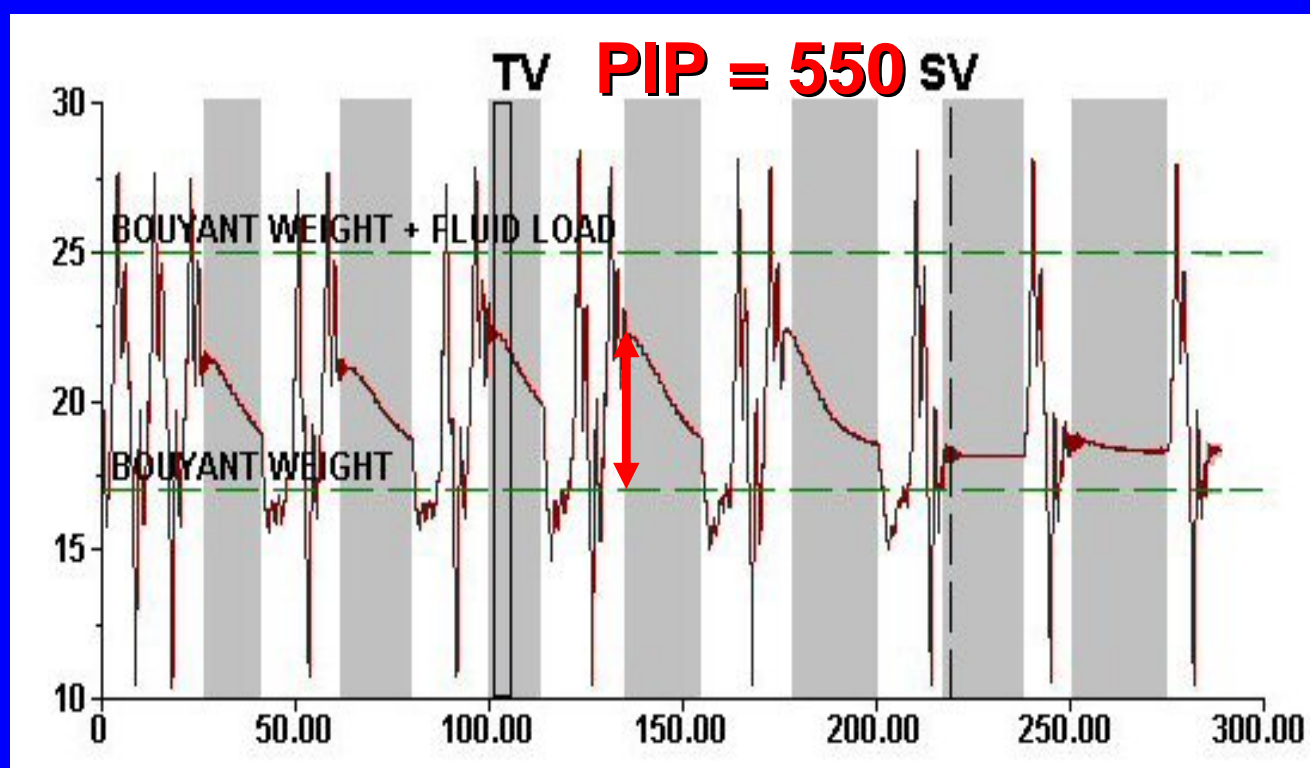
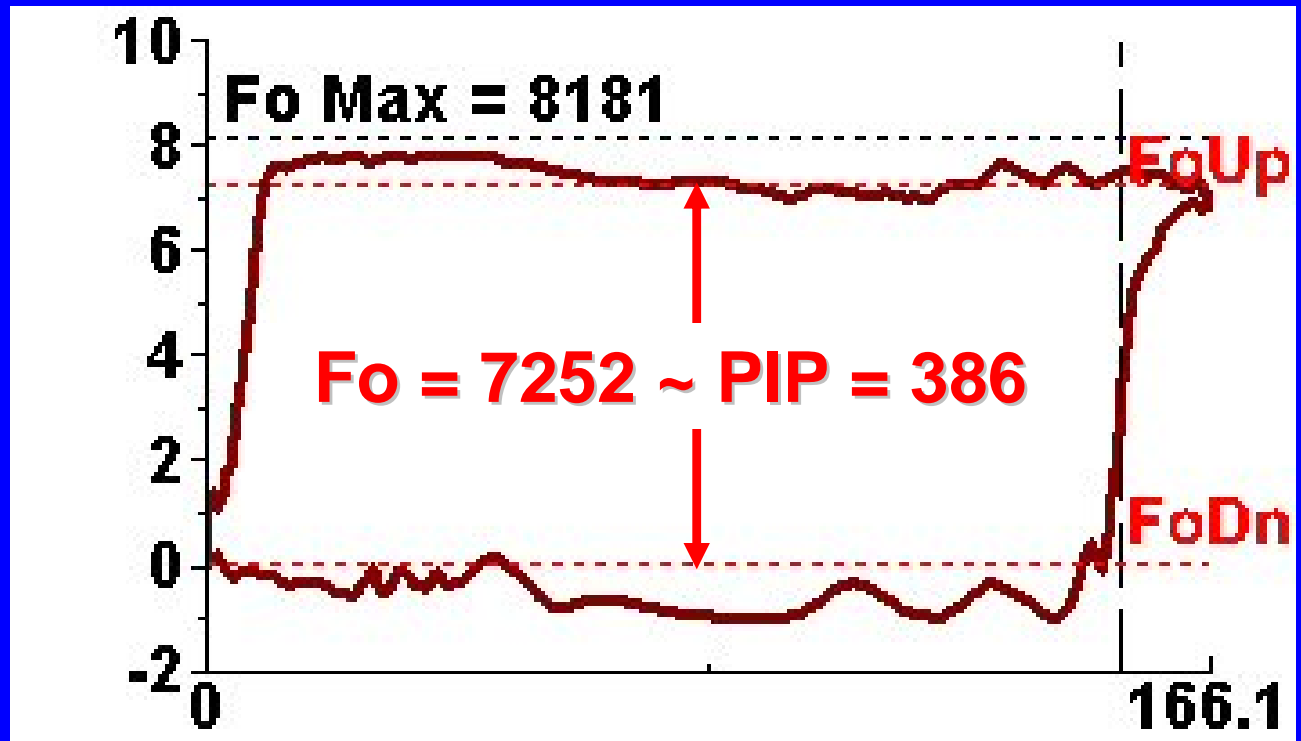


# 18 - PFL DHM Casing Weight Change



$Fo(fl) = 7457$   
 $Fo(pc) = 7252$   
 $Fo(vc) = 6857$

**PIP = 287**



# Pump Intake Pressure (Exclude Valve Check PIPs)

- 1) Average Error (PIP – Avg) = 242 Psig
- 2) (Meas – Avg) / Avg = 0.8% – 81.6% Avg 30.5%
- 3) Improved Average Error from 436 Psig

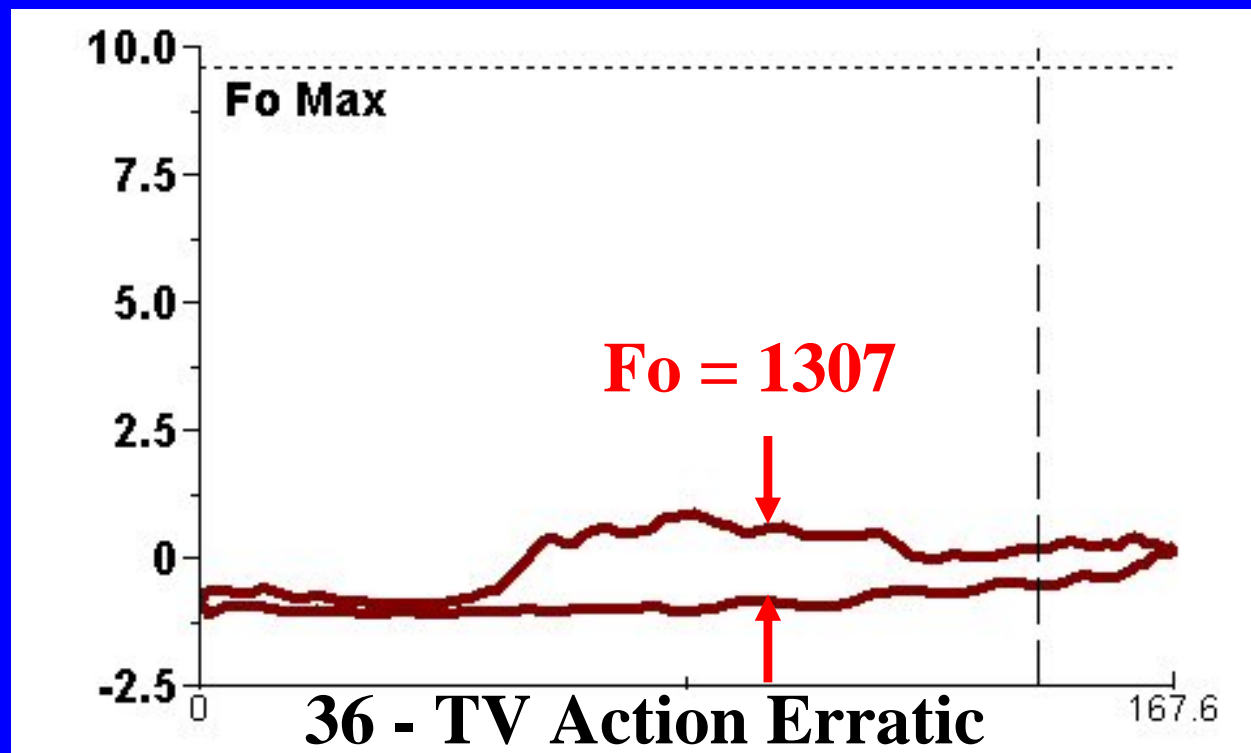
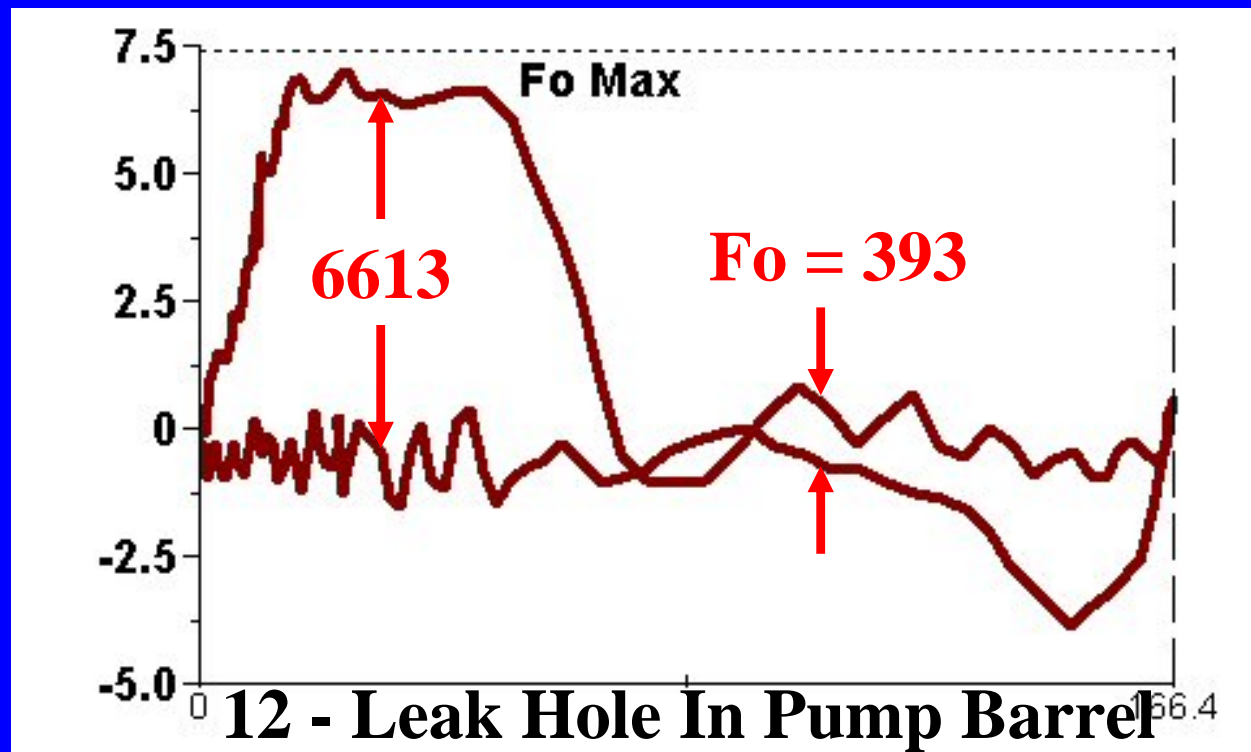
#	Example Dataset Well Name	DYNO Data				Average PIP Psig	Abs Max Error %	Abs Max Error Psig
		D	A	D	V			
38	V11	HT 3 1	62	66	43	64	3.3	2.1
33	Tagging Unanchored	L 1	63	54	187	58	8.0	4.7
37	Unaccounted Wellbore Friction	HT 1	341	330	18	335	1.6	5.4
9	Gas Interference	L 1	722	735	647	728	0.8	6.2
10	GearboxBalance	HT 1	827	810	1649	819	1.0	8.5
2	Anchored With Rod Stretch	HT 47	176	118	543	147	19.6	28.9
35	Trash Sticks TV Open	HT 1 12	305	365	1228	335	8.9	29.8
7	FluidPoundUnAnchoredTubing	L 2 1	45	110	58	78	41.5	32.3
18	PFL_DHM_CasingWtChange	HT 1	287	386	550	336	14.8	49.9
16	Need Gas Separator	HT 1	228	117	272	173	32.1	55.6
32	Tagging Fiberglass Rods on Downstroke	HT 2 1	339	58	58	198	70.7	140.3
1	Anchored but NOT Set	L 1	400	65	165	233	72.0	167.5
5	Bad Tail Bearing	L 2 1	568	955	732	762	25.4	193.3
3	Asphaltenes in Pump	L 2	527	1545	1523	1036	49.1	509.0
36	TV Action Erratic	L 1	623	2318	2303	1471	57.7	847.8
12	Leak Hole In Pump Barrel	HT 1	405	3990	4492	2197	81.6	1792.4

# Improved Calc Intake Pressures by Excluding:

Problems Due to:  
Asphaltenes in Pump  
TV Action Erratic  
Hole In Pump Barrel

Result in:

- 1) High Fluid Level
- 2) Erratic Pump Loads
- 3) Not Representative



# Pump Intake Pressure (Exclude Dyno w/ Problems)

- 1) Average Error (PIP – Avg) = 55.7 Psig
- 2) (Meas – Avg) / Avg = 0.8% – 72% Avg 23.1%
- 3) Best Match at Lower Pump Intake Pressures

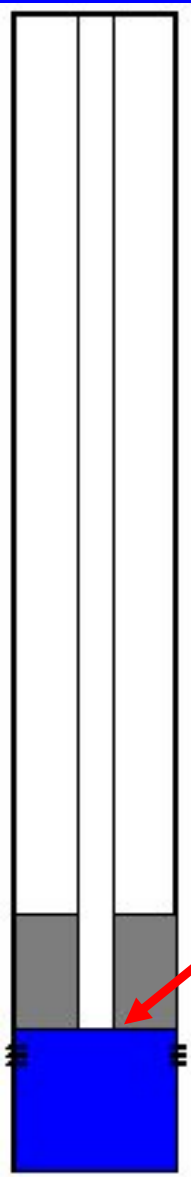
#	Example Dataset Well Name	DYNO Data				Average PIP Psig	Abs Max Error %	Abs Max Error Psig
		D	A	D	V			
38	V11	HT 3 1	62	66	43	64	3.3	2.1
33	Tagging Unanchored	L 1	63	54	187	58	8.0	4.7
37	Unaccounted Wellbore Friction	HT 1	341	330	18	335	1.6	5.4
9	Gas Interference	L 1	722	735	647	728	0.8	6.2
10	GearboxBalance	HT 1	827	810	1649	819	1.0	8.5
2	Anchored With Rod Stretch	HT 47	176	118	543	147	19.6	28.9
35	Trash Sticks TV Open	HT 1 12	305	365	1228	335	8.9	29.8
7	FluidPoundUnAnchoredTubing	L 2 1	45	110	58	78	41.5	32.3
18	PFL_DHM_CasingWtChange	HT 1	287	386	550	336	14.8	49.9
16	Need Gas Separator	HT 1	228	117	272	173	32.1	55.6
32	Tagging Fiberglass Rods on Downstroke	HT 2 1	339	58	58	198	70.7	140.3
1	Anchored but NOT Set	L 1	400	65	165	233	72.0	167.5
5	Bad Tail Bearing	L 2 1	568	955	732	762	25.4	193.3
3	Asphaltenes in Pump	L 2	527	1545	1523	1036		
36	TV Action Erratic	L 1	623	2318	2303	1471		
12	Leak Hole In Pump Barrel	HT 1	405	3990	4492	2197		

# Calculated Intake Pressures

## Improved by:

38 - V11 .....	Normal Well, OK
33 - Tagging Unanchored .....	Pumped Off, Fluid Level at Pump
37 - Unaccounted Wellbore Friction ..	Adjusted Pump Card, Fo
9 - Gas Interference .....	Adjusted Tubing Fluid Gradient
10 - Gearbox Balance .....	Normal Well, OK
2 - Anchored With Rod Stretch .....	Manually selected collar interval
35 - Trash Sticks TV Open .....	dPdT not correct, changed(0.7 to 0.3)
7 - FluidPoundUnAnchoredTubing .	Use defaults for FoUp and FoDn
16 - Need Gas Separator .....	User selected FoUp Load
18 - PFL_DHM_CasingWtChange ..	User selected FoUp Load
32 - Tagging Fiberglass Rods on ... Downstroke	Average Joint Length incorrect, too high of PFL (Exclude Data)
1 - Anchored but NOT Set .....	User selected FoUp and FoDn
5 - Bad Tail Bearing .....	Avg of Downstroke Loads, change tubing gradient from 0.412 to 0.38

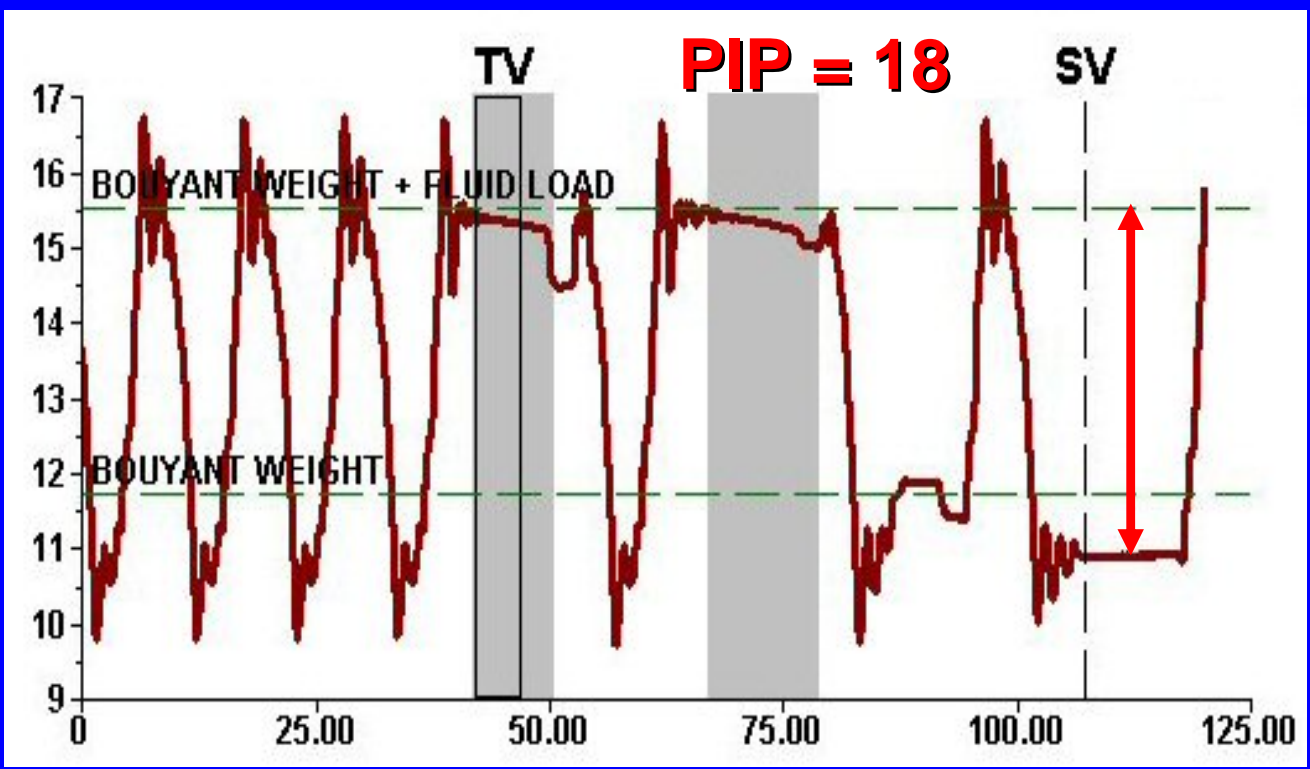
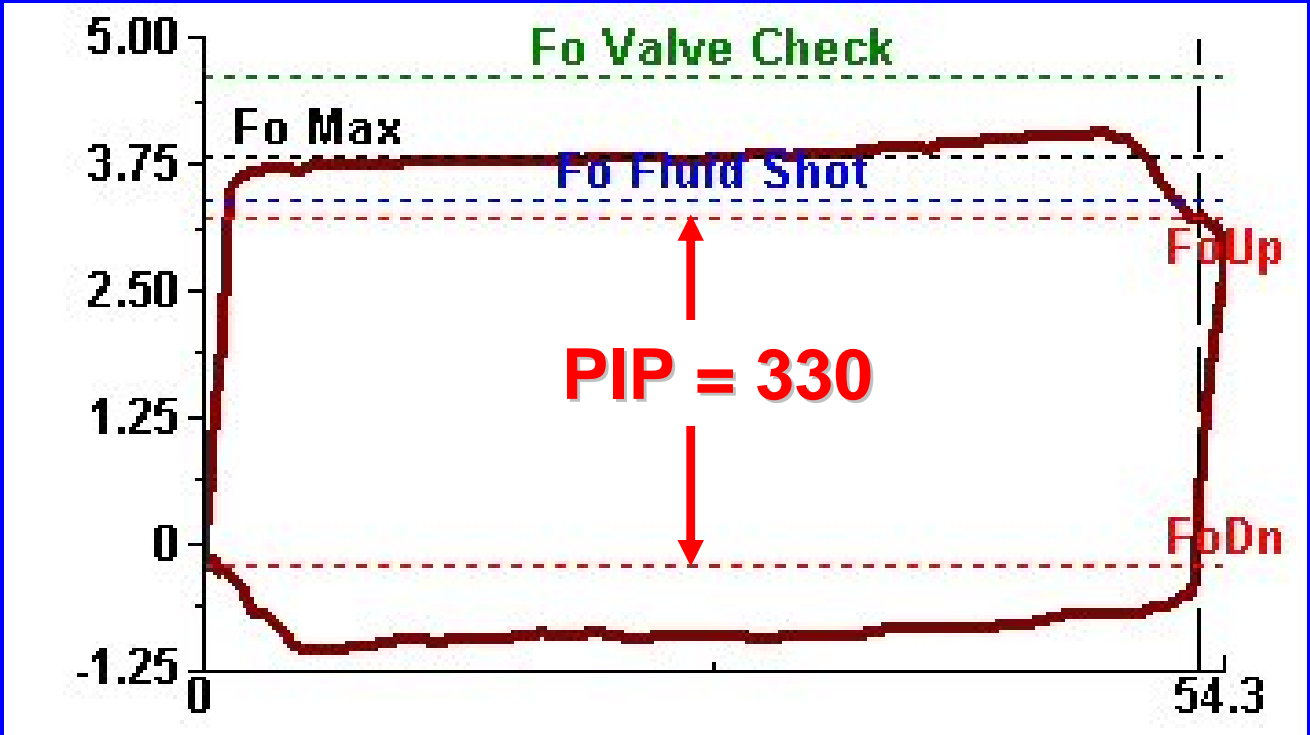
# 37 - Unaccounted Wellbore Friction



**2.25" = 3.98 in<sup>2</sup>**

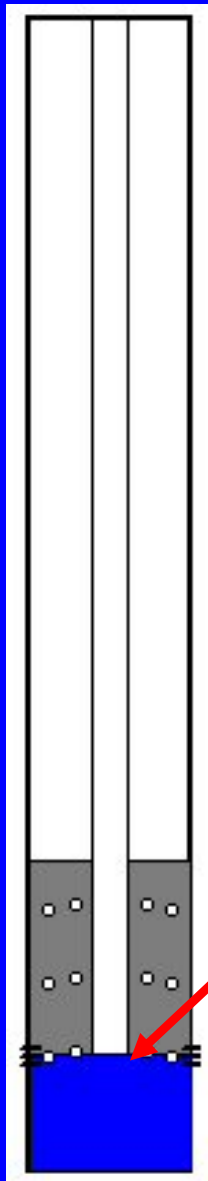
**Fo(fl) = 7457**  
**Fo(pc) = 7252**  
**Fo(vc) = 6857**

**PIP = 341**





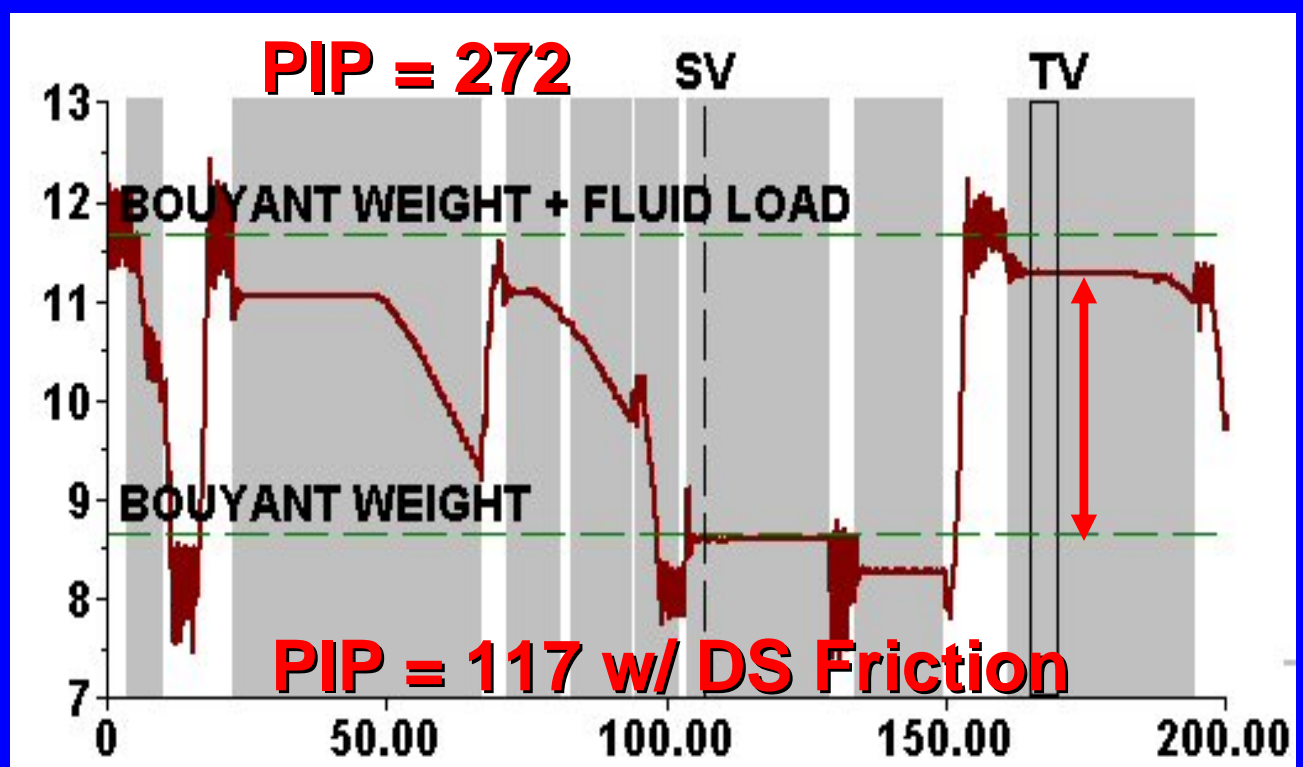
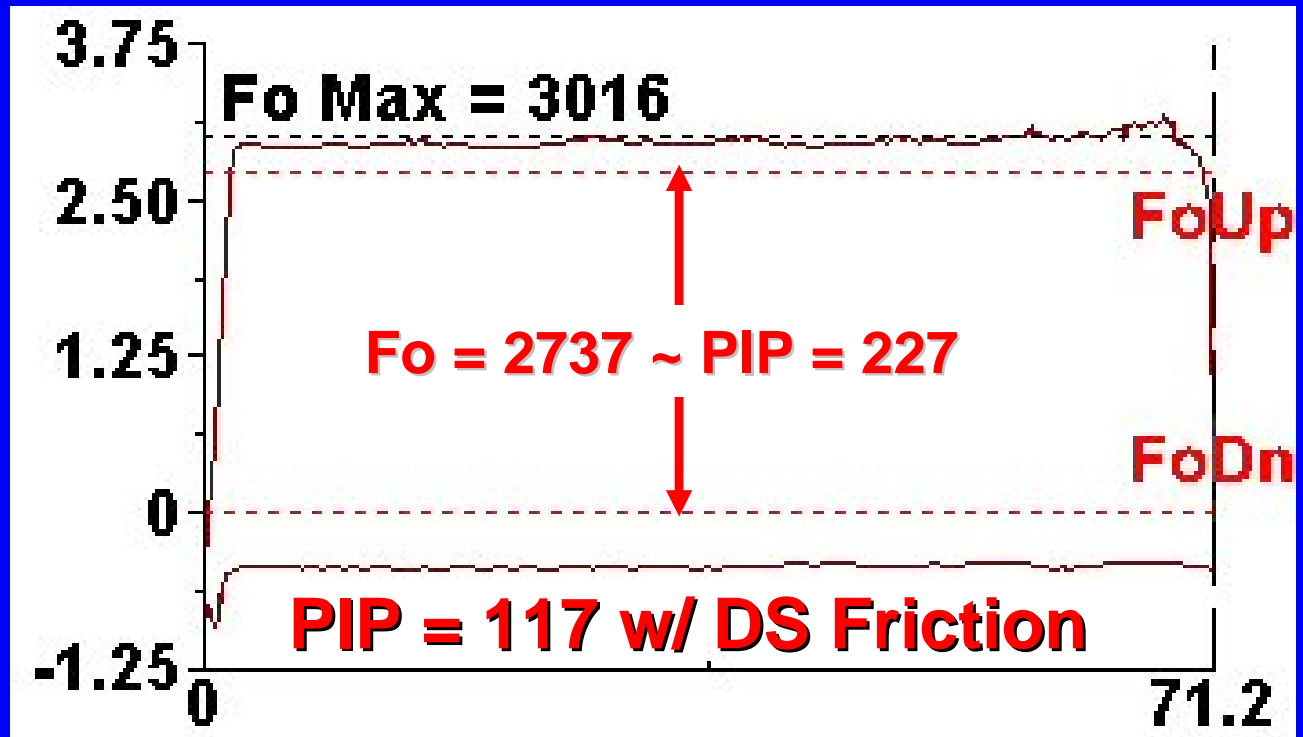
# 16 – Need Gas Separator



1.25" = 1.22 in<sup>2</sup>

Fo(fl) = 2718  
 Fo(pc) = 2737  
 Fo(vc) = 2682

PIP = 228





# Corrected Calculation of Pump Intake Pressures

1) Average Error (PIP – Avg) = 4.5 Psig

2) (Meas – Avg) / Avg = 0.1% – 12% Avg 3.0%

3) Improved Average Error from 436 Psig

#	Example Dataset Well Name	DYNO Data				Average PIP Psig	Abs Max Error %	Abs Max Error Psig
		A	D	D	V			
38	V11	HT 3 1	62	66	43	64	3.3	2.1
33	Tagging Unanchored	L 1	63	54	187	58	8.0	4.7
37	Unaccounted Wellbore Friction	HT 1	341	330	18	335	1.6	5.4
9	Gas Interference	L 1	722	735	647	728	0.8	6.2
10	GearboxBalance	HT 1	827	810	1649	819	1.0	8.5
2	Anchored With Rod Stretch	HT 47	127	118	543	123	3.5	4.3
35	Trash Sticks TV Open	HT 1 12	352	365	1228	358	1.8	6.4
7	FluidPoundUnAnchoredTubing	L 2 1	45	35	58	40	12.7	5.1
16	Need Gas Separator	HT 1	228	227	272	228	0.3	0.7
18	PFL_DHM_CasingWtChange	HT 1	287	301	550	294	2.5	7.3
32	Tagging Fiberglass Rods on Downstroke	HT 2 1	339	58	58	198		
1	Anchored but NOT Set	L 1	400	401	165	401	0.1	0.4
5	Bad Tail Bearing	L 2 1	568	562	564	565	0.6	3.4
3	Asphaltenes in Pump	L 2	527	1545	1523	1036		
36	TV Action Erratic	L 1	623	2318	2303	1471		
12	Leak Hole In Pump Barrel	HT 1	405	3990	4492	2197		

# Accuracy of PIP from Dynamometer Measured Loads Depends On

- 1) Load cell damaged
- 2) Calibration of the load cell
  - Zero Offset and Hysteresis
  - Not centrally loaded
- 3) Pump card shifted off the zero load line
- 4) Specifying a tubing fluid gradient, difficult in wells that flow or have lots of gas.
- 5) Unaccounted friction: deviated wells, tight stuffing boxes, bottled up pumps, or paraffin
- 6) Bad/Missing Input Data

**15000 lbs x 1% x 1.50' Plunger = 85 psi**

# **Accuracy of PIP from Fluid Levels Depends On**

- 1) Can't shoot Fluid level when Pumping Below Packer**
- 2) User Frequently does not Verify Input Data**
  - **Default Avg. Joint Length**
  - **Other Missing Data**
- 3) Gaseous Liquid ? for very high Fluid Levels, CO2 and Viscous Crude**
- 4) Operator does not review and verify analysis done automatically by software**

**Fluid Level off by 1 joint = 11 psi**

# Conclusions

- 1) **Should not accept default analysis for PIP**
  - **Initial Average PIP Error was 436 psi**
  - **Initial Maximum Error was 2556 psi**
- 2) **Error impacts PIP differently**
  - **Fluid Level Off by 1 Tubing Joint ~ 11 Psi**
  - **1% Error in Dyno Load ~ 85 psi Error**
- 3) **PIP from Valve Checks most Error**
- 4) **PIP from Pump Card in the Middle**
- 5) **PIP from Fluid Level has Least Error**
  
- 6) **Proper Analysis Results in Accurate PIP**